



# Efficient Removal of Lead and Arsenic from Groundwater Using Thiourea-Modified Biochar and Nano Zerovalent Zinc

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## Abstract

Groundwater contamination by heavy metals such as lead (Pb) and arsenic (As) is a critical environmental and public health issue due to their toxicity and persistence. This study investigates a sustainable and low-cost approach using rice husk-derived biochar modified with thiourea (TMBC) and combined with nano zerovalent zinc (nZVZn) to enhance removal efficiency through adsorption and redox reactions. Batch experiments assessed the effect of pH (3–9), contact time (5–180 min), adsorbent dosage (0.05–0.5 g), and initial metal concentration (10–100 mg/L) on removal performance. The nZVZn–TMBC composite achieved over 90% Pb and 85% As removal at optimal pH values of 5 and 6–7, respectively, reaching equilibrium within 90 minutes. Adsorption followed Langmuir isotherm behavior, indicating monolayer coverage, and pseudo-second-order kinetics suggested chemisorption as the dominant mechanism. Material characterization confirmed successful thiourea functionalization and uniform nZVZn deposition, providing increased surface area (215 m<sup>2</sup>/g) and abundant active sites. The approach demonstrates effective heavy metal remediation, utilizing agricultural waste and a green synthesis strategy, offering a practical solution for groundwater treatment in resource-limited settings. Future studies should focus on field-scale application, adsorbent regeneration, and multi-contaminant treatment.

## KEYWORDS

Fiber traits, Multivariate analyses, Cotton genotypes.

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## 1 | INTRODUCTION

Underground water is a major resource. It significantly contributes to drinking water, agricultural irrigation, and industrial processes. Moreover, it constitutes 25% – 40% of the world's drinking water (Krishnakumari et al. 2018). Groundwater is threatening due to natural processes and human activities that cause deterioration of its quality. There are natural sources like geological leaching. There are also man-made sources like industrial discharges, improper waste disposal, agricultural runoff (Kanmani & Gandhimathi, 2012). Substances that are hazardous to human health are called toxicants. Heavy metal contaminants, especially lead (Pb) and arsenic (As), are of serious concern due to being toxic, non-biodegradable and bio-accumulative (Lee et al. 2009).

The problem of water contamination is being aggravated by urbanization and industrialisation. Contamination due to nitrate, chlorides, and heavy metals are often seen in places. And, these are places where human activities are large. The presence of industrial contaminants, such as petroleum hydrocarbons and organic solvents, complicates the remediation process and causes further damage (Cho et al., 2004). The groundwater pollution near the landfills is very high because leachates migrate and transfer toxic chemicals into the aquifers (Aweto & Ovwamuedo, 2023).

Impure substances like Pb and As have an adverse effect on the body. They can cause severe neurology-related disorders, kidney damage and increase cancer risks. Moreover, consuming water containing them can expose people to their harmful effects over the years (Rahman & Singh, 2019). Polluted Pb often comes from industrial activities such as smelting and the corrosion of lead plumbing (Levin et al., 2021). On the contrary, arsenic dissolves into groundwater, arising from minerals that bear arsenic. In addition, it is being released due to human activities, Jha and Tripathi wrote in 2021.

According to Caroline *et al.* (2017), it is not easy to remediate the heavy metal contamination as conventional water treatment methods fail to remove their traces from the water. Due to this, interest towards alternative and more effective remediation technologies such as biochar and nano zero-valent zinc (nZVZn) has increased. Biochar has a high surface area and various functional groups, which make it a good adsorbent for heavy metals. Liu and Zhang (2022) reports that it is an effective Pb and As remover. However, Zhu et al. 2020 observe that modifications that allow better binding through chemicals such as thiourea-modified biochar (TMBC) will enhance the functionality and adsorption capacity of adsorbents.

The combination of nZV Zn and biochar can achieve great success in cleaning up the environment owing to the high reactivity of nZV Zn, which reduces metal ions to less toxic form through redox reaction (Li *et al.*, 2016). The capacities of TMBC and nZVZn cooperate with each other; thus, TMBC nZVZn can be an effective strategy to remove. The inclusion of TMBC improves the nZVZn stability and adsorbent capacity for effectively reducing Pb and As contaminants, especially in saline environments (Macedo *et al.*, 2021; Duan *et al.*, 2020).

The subterranean water pollution issue is critical, and conventional treatment is limited. This research aims to study nZVZn-modified biochar and thiourea-modified biochar for arsenic and lead taking from sub-surface water. We will optimize the operational conditions like pH, time, initial metal concentration and dosage in order to remove the toxic metals efficiently.

## 2 MATERIALS AND METHODS

### Preparation of Adsorbents

#### Rice Husk Biochar

Rice husk was used to prepare biochar. Cleaning husks with distilled water to remove dirt followed by drying at room temperature for 24 hours. The biomass was pyrolyzed in a muffle furnace within a temperature of 350–450°C for 3 hours and under limited oxygen environment. This ensured that the biomass was partially carbonized while still retaining oxygen-functional groups that are critical for adsorption of metals (Asadi *et al.*, 2021). After being pyrolyzed, the biochar was milled, passed through a 0.5 mm sieve and kept in an airtight container to avoid moisture absorption, before being modified and tested (Fig 1).

#### Nano Zerovalent Zinc (nZVZn)

They made nano zerovalent zinc through a process called chemical reduction. A precursor solution was prepared from 1.5 g zinc chloride ( $ZnCl_2$ ) in 4:1 ethanol: deionized water mixture. The  $ZnCl_2$  solution came under magnetic stirring and dropwise addition of Sodium borohydride ( $NaBH_4$ ) (Fig 1). The black substance formed confirms the presence of nZVZn. The particles were isolated by centrifugation, washed by trichloroethanol, dried at 60°C for six hours and then kept in a desiccator (Saleh, 2024).



**Fig. 1:** Rice husk biochar and Nano zerovalent Zinc

### Preparation of nZn-Modified Biochar

Biochar was first prepared as described above to synthesize nZn-modified biochar (nZn-BC). 4:1 (v/v) 51% ethanol-water mixture was used to dissolve ZnCl<sub>2</sub> (zinc chloride) and a reducing agent NaBH<sub>4</sub> (sodium borohydride) was utilized to prepare the hot zinc chloride solution. The solution of NaBH<sub>4</sub> was added slowly to ZnCl<sub>2</sub> and stirred under nitrogen to prevent oxidation of the mixture. After the reduction, 1 g of biochar was added and stirred for 2 hours to evenly distribute the ZnNPs on the biochar. The composite obtained was filtered followed by washing with ethanol and deionized water before oven-drying it at 70 °C for 12 hours. This new hybrid material has shown better adsorption and redox properties which can be used to remove metals (Ahmad *et al.*, 2014; Duan *et al.*, 2020).

### Preparation of Thiourea-Modified Biochar (TMB)

Thiourea modified biochar for enhancing adsorption capacity. A total of one gram of biochar was mixed with 20 mL thiourea solution (1N) and heated at 40°C in a water bath for 6 hours. The addition of sulfur and nitrogen groups on the surface of biochar enables it to bind with heavy metals through ion exchange as well as chelation (Zhu *et al.*, 2020; Fei & Hu, 2022). The biochar which was modified was subjected to filtration, dried overnight at 70°C and stored in desiccators.

### Batch Sorption Experiments

The adsorption capacity of the prepared adsorbents (biochar, TMB, nZn, and TMB-nZn composite) toward the removal of lead (Pb) and arsenic (As) was conducted via batch sorption tests. A mass of 0.1 g of each adsorbent was added to 50 mL of a solution of known metal concentrations. The mixture got shaken at 150 rpm for uniform contact. Samples at given time interval were collected, filtered through 0.45 µm membrane and analyzed using atomic absorption spectroscopy (AAS) for metal concentration (Zhu *et al.*, 2020; Khanzada *et al.*, 2023).

### Effect of pH

The pH solution is also importantly influence on the adsorption of metal. Sorption tests were done at pH 3 to 9 to help find the best pH for removing Pb<sup>2+</sup> and As<sup>5+</sup>. We used 0.1 M NaOH and 0.1 M HCl to adjust pH. The maximum adsorption of lead was observed at pH 5–6, while the most favorable pH for arsenic removal was at 6.5–7.5 (Zhu *et al.*, 2020; Singh *et al.*, 2023).

### Effect of Contact Time

Contact time experiments were conducted to determine the rate of metal adsorption and equilibrium time. Contact times ranged from 5 to 180 minutes, with samples taken periodically to track the kinetic progress of metal removal. The data reveals that adsorption occurs very rapidly within the first 30 minutes, whereas equilibrium was achieved at 60–120 minutes. This is an indication that a chemisorption has occurred and the data fits pseudo-second order kinetics (Ho & McKay, 1999).

### Effect of Sorbent Dosage

The amount of sorbent for metal removal was varied by changing the adsorbent quantity between 0.05 g to 0.5 g in 50 mL of contaminated water. When the dosage increased, removal efficiency also improved. However, the rate of the improvements plateaued at doses above 0.3 g. This was likely due to particle agglomeration and limited available surface area (Zhang *et al.*, 2022).

### Effect of Initial Metal Concentration

The ability to absorb also examined for beginning metals concentrations that were between 10 mg/L and 100 mg/L. Increased concentrations of metals enhanced their uptake (mg/g). However, the removal efficiency shows a declining trend due to site saturation for concentrations higher than 60 mg/L. (Carolin *et al.*, 2017; Ouyang *et al.*, 2024) Monolayer adsorption with finite binding capacity observed by Langmuir isotherm modeling (Chen *et al.*, 2018).

### Modeling: Kinetic and Isotherm Studies

To identify the rate-determining steps pseudo-first-order and pseudo-second-order models were applied to the

adsorption kinetics. The model that best describes the adsorption phenomena observed (pseudo-second-order kinetics) suggests that the processes are chemisorption which takes place via exchange of electrons between adsorbent and adsorbate (Ho & McKay, 1999). Langmuir and Freundlich Isotherms were used to describe the adsorption. Langmuir best represented the monolayer adsorption and finite adsorption sites, whilst Freundlich depicts surface heterogeneity.

### 3 RESULTS

#### SEM Characterization of adsorbents

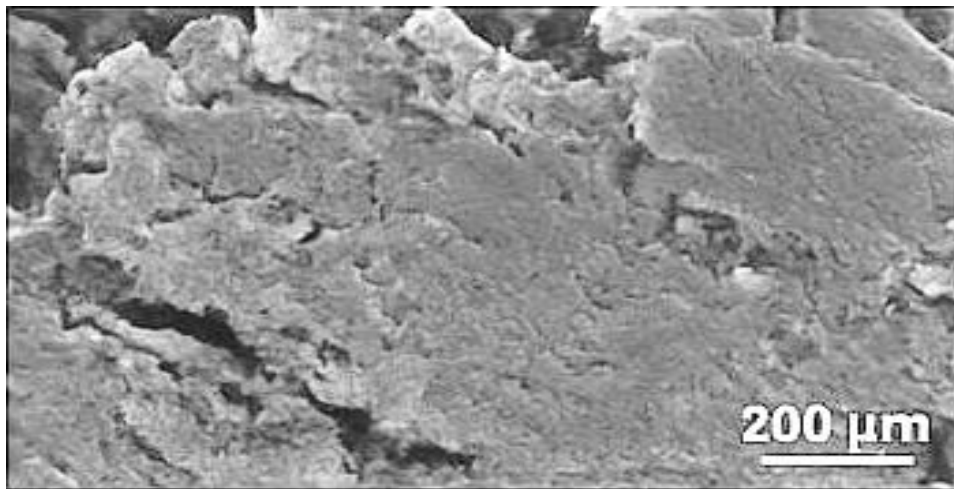
##### Characterization of rice husk biochar

The image features a scale bar of 200  $\mu\text{m}$  the structures observed were in the micron range (micro-porous to meso-porous structures). A SEM image showed a rough uneven surface having voids and cavities. Figure 2 shows biochar made from burning agri waste (rice husk) material at high heat.

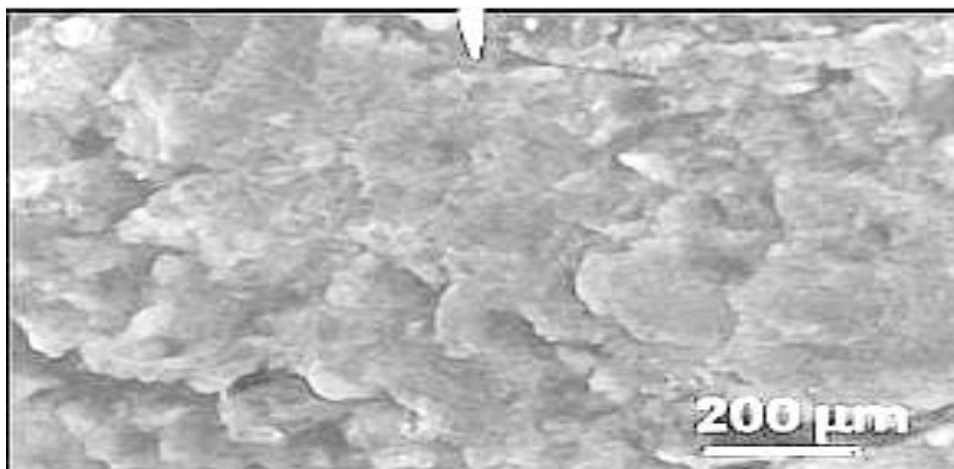
The presence of many pores and cracks indicates a high surface area essential for adsorption. The uneven and stratified structure advised that the organic material was partly carbonized, with active useful functional groups (carboxyl, hydroxyl etc.) present on the biochar surface that were already adsorbed metal ions present in the material. The RH-BC material, which has a rough and porous surface, presented good adsorptive capacity for the removal of heavy metals from contaminated water, as its surface had more binding sites.

##### Characterization of Thiourea Modified Biochar

Compared to unmodified rice husk biochar, the surface of thiourea modified biochar was denser and smoother with fewer large pores visible. Particles and surface features tend to be clumped together and smooth after chemical modification (Fig 3).



**Fig. 2:** SEM image of rice husk-derived biochar (RH-BC) displaying heterogeneous surface topography characterized by porous networks and cavities.



**Fig. 3:** SEM image of TMBC displaying modified surface topography with increased density and uniformity compared to unmodified biochar.

Surface functionalization nitrogen and sulfur-containing functional groups (such as thiol  $-SH$  and amine  $-NH_2$  groups). Partial blocking or filling of pores which explained the more compact surface, as well as creating additional chemical binding sites. Although the large pores seem fewer in number, surface chemistry is more reactive enabling better chemisorption of heavy metals such as  $Pb^{2+}$  and  $As^{3+}$  ions through complexation with the functional groups.

#### Characterization of zinc modified biochar (TMBC)

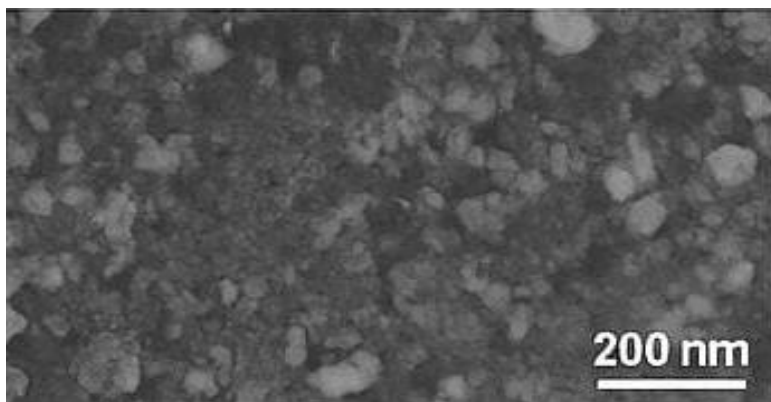
White/grey dots representing discrete nanoparticles dispersed and deposited on the biochar surface. These were nano zerovalent zinc (nZVZn) particles, likely in the  $\sim 20\text{--}100$  nm size range. The base of the biochar appears as a dark, unbroken matrix offering support to the Zn nanoparticles. The nanoparticles appeared to be well dispersed essential to maximizing surface reactivity. Uniformly dispersed nZVZn particles increase active surface area for adsorption and reduction of heavy metals. The nZVZn particles had high reductive capacity they have the capability of chemically reducing and immobilizing  $Pb^{2+}$  and  $As^{3+}$  ions. Aside from the functionalized and porous biochar matrix, the composite material also includes synergistic pollutant removal by redox and adsorption (Fig 4).

#### Characterization of zinc based nano particles (nZVZn)

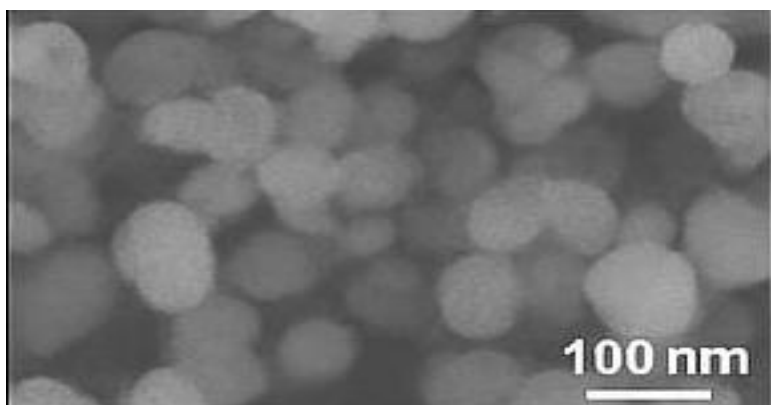
Sub-spherical to spherical particles with a diameter of 20-80 nm and metallic, smooth surface. Highly even size distribution with moderate agglomeration of particles.

Large surface-to-volume ratio to be more reactive. Metallic zinc ( $Zn^0$ ) was highly electron-donating Excellent SEM contrast verified excellent electrical conductivity.

Suitable for heavy metal remediation via reduction mechanisms, especially for the elimination of Pb, As, and Cr from polluted water (Fig 5).



**Fig. 4:** Scanning electron microscopy of nZVZn-BC composite revealing well-dispersed nano zerovalent zinc particles (luminous features) integrated within the biochar framework.



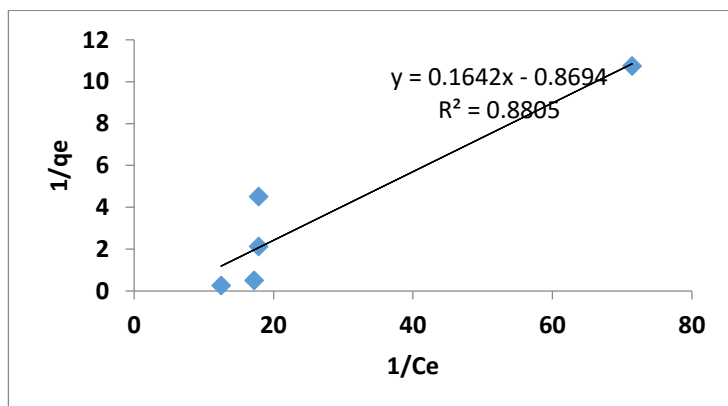
**Fig. 5:** SEM image of nZVZn particles exhibit spherical morphology with 20-80 nm diameter and uniform dispersion, confirming successful synthesis suitable for water treatment applications.

#### Sorption Isotherm Modeling for Lead and Arsenic Removal using Rice Husk-Biochar (RH-BC)

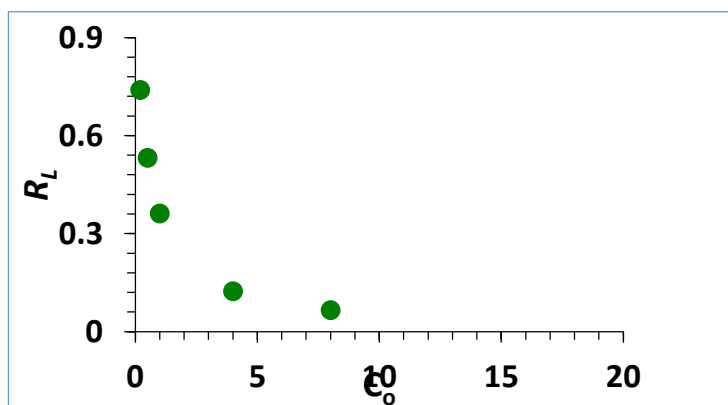
Four parameters of nonlinear isotherm models were used to describe the sorption process of lead (Pb) and arsenic (As) using rice husk-biochar (RH-BC) namely Langmuir, Freundlich, Temkin and Dubinin-Radushkevich as shown in the figure.

## Langmuir Model Analysis

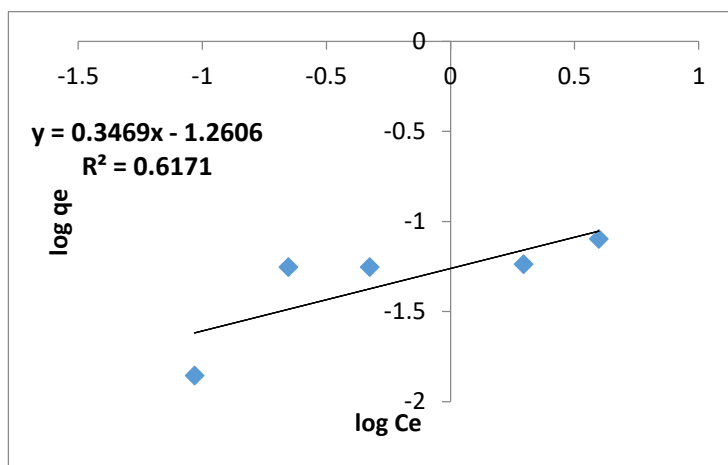
The Langmuir model shown good fit for lead and arsenic removal using RH-BC with  $R^2 = 88.05\%$  and maximum sorption capacity ( $q_m$ ) value of 6.09 mg/g. The separation factor ( $K_L$ ) value was 0.19 L/g, indicating favorable sorption conditions. Figure 4.5 shown the Langmuir model fit for RH-BC sorbent. The Langmuir constant calculated from the slope was 0.164, and the intercept value was 0.87. The separation factor ( $K_L$ ) was calculated to explore the favorability of Pb and As sorption onto RH-BC, which shown that sorption is favorable using this sorbent with RL values ranging from 0.07 to 0.74 across different initial concentrations (0.2 to 8 mg/L) (Fig 6a, 6b).



**Fig. 6a:** Freundlich isotherm linear plot for adsorption of Pb(II)/As(III) showing the relationship between  $1/q_e$  and  $1/C_e$ . The regression line ( $y = 0.1642x - 0.8694$ ) with  $R^2 = 0.8805$  indicates a good model fit.



**Fig. 6b:** Dubinin-Radushkevich (D-R) isotherm plot for adsorption of Pb(II)/As(III) onto biochar, nZVZn, thiourea-modified biochar, and nZVZn-TMBC composites.



**Fig. 7:** Freundlich isotherm model for Pb(II)/As(III) adsorption showing the linear relationship between  $\log q_e$  and  $\log C_e$ , with correlation coefficient ( $R^2 = 0.6171$ ).

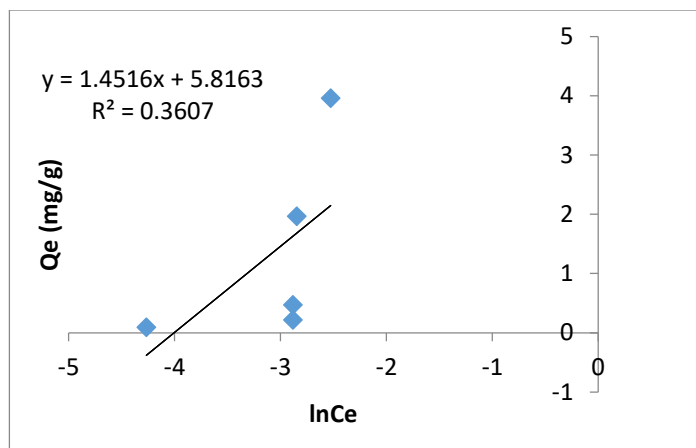
## Freundlich Model Analysis

The Freundlich model (non-linear) was employed for RH-BC showing  $R^2 = 61.71\%$ . The Freundlich constant ( $K_F$ ) value was 18.22  $\text{mg}^{(1-n)} \text{g}^{-1} \text{L}^n$ , indicating good sorption capacity. The sorption intensity coefficient ( $1/n$ ) was 0.35, which is less than 1, confirming favorable sorption conditions. The  $n$  value of 2.88 suggests that the

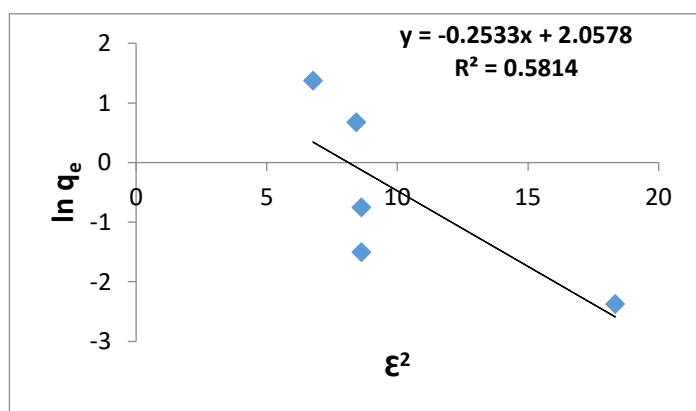
sorption process follows a favorable isotherm pattern. Figure 7 demonstrated the Freundlich model fit for RH-BC. The slope of 0.347 and intercept of 1.26 were used to calculate the Freundlich parameters. The decrease in the  $1/n$  value explained that the sorption potential remained consistent across varying initial concentrations of Pb and As.

### Temkin Model Analysis

The Temkin model shown lower fit with  $R^2 = 36.07\%$  for RH-BC. The heat of sorption ( $b$ ) was calculated as 1707 J/mol, indicating moderate to high binding energy between the adsorbate and RH-BC surface. The Temkin equilibrium binding constant ( $AT$ ) was 54.97 L/g, suggesting good affinity between the metal ions and RH-BC surface. Figure 8 shown the Temkin model plot for RH-BC. The slope of 1.45 and intercept of 5.82 were used to determine the Temkin constants. This heat of sorption value indicates that the sorption process involves both physical and weak chemical interactions, with stronger binding compared to purely physical adsorption.



**Fig. 8** Temkin isotherm model for Pb(II)/As(III) adsorption, illustrating the linear plot of  $q_e$  versus  $\ln C_e$  with correlation coefficient ( $R^2 = 0.3607$ ).



**Fig. 9:** Dubinin–Radushkevich (D–R) isotherm model for Pb(II)/As(III) adsorption, showing the linear plot of  $\ln q_e$  versus  $\epsilon^2$  with correlation coefficient ( $R^2 = 0.5814$ ).

### Dubinin-Radushkevich Model Analysis

The Dubinin-Radushkevich model provided moderate fit for the sorption data with  $R^2 = 58.14\%$ . The theoretical sorption capacity ( $q_D$ ) was calculated as 7.83 mg/g. The bonding energy  $\epsilon$  was calculated to be 3.48 kJ/mol, which is less than 8 kJ/mol but significantly higher than typical physical sorption values, indicating that the sorption mechanism involves both physical and weak chemical interactions. Figure X.X illustrated the Dubinin-Radushkevich model fit for RH-BC. The slope of -0.253 and intercept of 2.06 were used to calculate the model parameters. This moderate bonding energy suggests that electrostatic interactions, hydrogen bonding, and weak chemical complexation contribute to the sorption process alongside van der Waals forces (Fig 9).

### Overall Isotherm Analysis

The overall isothermal modeling data shown the Langmuir model provided the best fit ( $R^2 = 88.05\%$ ) for Pb and As sorption using RH-BC, followed by Freundlich ( $R^2 = 61.71\%$ ) and Dubinin-Radushkevich ( $R^2 = 58.14\%$ ) models. The Temkin model shown the lowest correlation ( $R^2 = 36.07\%$ ). The mechanism of sorption was determined to

involve both physical and weak chemical interactions based on the calculated bonding energy of 3.48 kJ/mol from the Dubinin-Radushkevich model.

The good fit of the Langmuir model suggests predominantly monolayer adsorption on relatively homogeneous surface sites of the RH-BC, with a maximum sorption capacity of 6.09 mg/g. The favorable Freundlich parameters ( $n = 2.88$  and  $1/n = 0.35$ ) indicate that the sorption process is favorable and that multilayer adsorption may occur at higher concentrations. The higher bonding energy compared to purely physical sorption suggests that functional groups present on the biochar surface, such as hydroxyl, carboxyl, and phenolic groups, contribute to the sorption mechanism through weak chemical interactions.

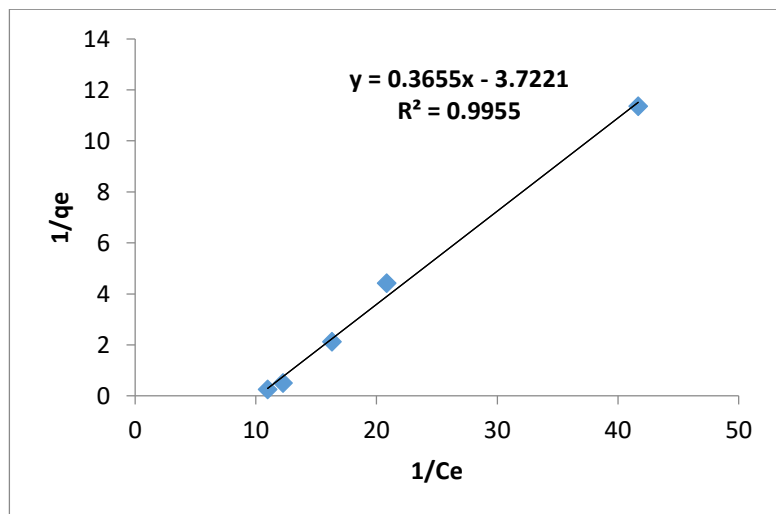
The sorption mechanism can be attributed to the porous structure of rice husk-biochar and the presence of various functional groups that facilitate both electrostatic attraction and weak chemical bonding with Pb and As species. The moderate bonding energy indicates that the process involves a combination of physical and chemical sorption mechanisms, which may offer advantages in terms of both sorption capacity and potential for regeneration. The reusability of the RH-BC should be further evaluated through desorption studies to determine the practical applicability of this treatment system for groundwater remediation.

### Sorption Isotherm Modeling for Lead and Arsenic Removal using nZVZn

Four parameters of nonlinear isotherm models were used to describe the sorption process of lead (Pb) and arsenic (As) using nano zerovalent zinc (nZVZn) and thiourea modified biochar namely Langmuir, Freundlich, Temkin and Dubinin-Radushkevich as shown in figure.

#### Langmuir Model Analysis

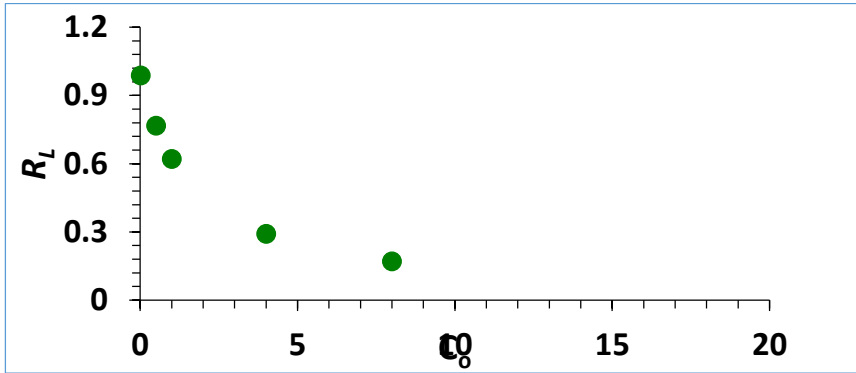
The Langmuir model shown excellent fit for lead removal using nZVZn with  $R^2 = 99.5\%$  and maximum sorption capacity ( $q_m$ ) value of 2.74 mg/g. The separation factor ( $K_L$ ) value was 0.098 L/g, indicating favorable sorption conditions. Figure X.X showed the best fit Langmuir model for nZVZn sorbent. The standard error was found to be minimal ( $SE \pm 0.28$ ), confirming the reliability of the model. The separation factor ( $K_L$ ) was calculated to explore the favorability of Pb and As sorption onto nZVZn, which showed that sorption is highly favorable using this sorbent (RL values ranging from 0.17 to 0.99) (Fig 10).



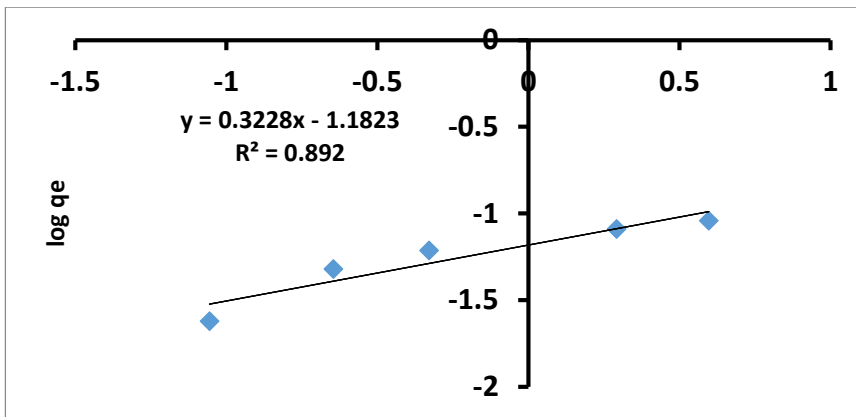
**Fig. 10:** Linearized Freundlich isotherm model for Pb(II)/As(III) adsorption showing the plot of  $1/q_e$  versus  $1/C_e$ . The regression equation ( $y = 0.3655x - 3.7221$ ) and high correlation coefficient ( $R^2 = 0.9955$ ) indicate a good fit of the experimental data to the model.

#### Freundlich Model Analysis

The Freundlich model (non-linear) was also employed for nZVZn showing  $R^2 = 89.2\%$  with standard error of  $\pm 0.45$ . The Freundlich constant ( $K_F$ ) value was  $15.22 \text{ mg}^{(1-n)} \text{ g}^{-(1-n)} \text{ L}^n$ , indicating good sorption capacity. The sorption intensity coefficient ( $1/n$ ) was 0.32, which is less than 1, confirming favorable sorption conditions. The  $n$  value of 3.10 suggests that the sorption process follows a favorable isotherm pattern. The decrease in the  $1/n$  value explained that the sorption potential remained consistent across varying initial concentrations of Pb and As (Fig 11, Fig 12).



**Fig. 11:** Dimensionless separation factor ( $R_L$ ) versus initial concentration ( $C_0$ ) plot based on the Langmuir isotherm. The  $R_L$  values between 0 and 1 indicate favorable adsorption, with decreasing  $R_L$  values at higher  $C_0$  suggesting enhanced adsorbate affinity at increased initial concentrations.



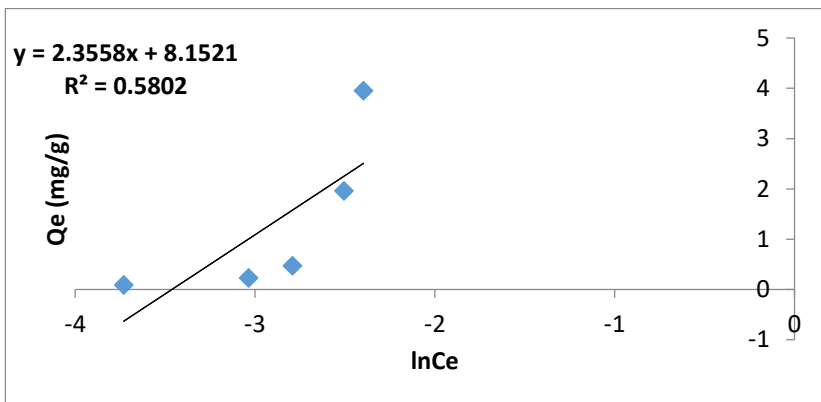
**Fig. 12:** Freundlich isotherm plot for Pb(II)/As(III) adsorption onto adsorbents showing the linear relationship between  $\log q_e$  and  $\log C_e$ . The good correlation coefficient ( $R^2 = 0.892$ ) indicates that the adsorption data fits well with the Freundlich isotherm model, suggesting multilayer adsorption with heterogeneous surface binding sites.

**Temkin Model Analysis**

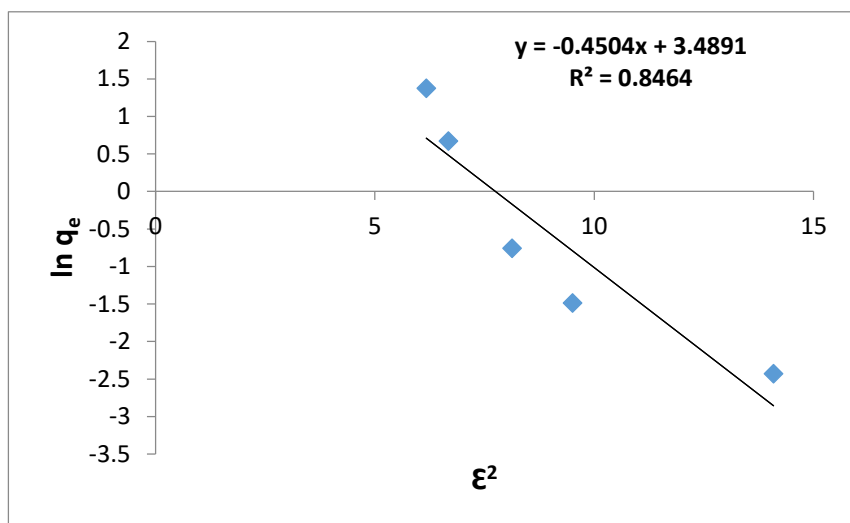
The Temkin model shown moderate fit with  $R^2 = 58\%$  for nZn. The heat of sorption ( $b$ ) was calculated as 1052 J/mol, indicating moderate binding energy between the adsorbate and adsorbent surface. The Temkin equilibrium binding constant ( $AT$ ) was 31.83 L/g, suggesting reasonable affinity between the metal ions and nZn surface. This heat of sorption value indicates that the sorption process involves both physical and weak chemical interactions (Fig. 13).

**Dubinin-Radushkevich Model Analysis**

The Dubinin-Radushkevich model provided good fit for the sorption data with  $R^2 = 84.6\%$ . The theoretical sorption capacity ( $q_D$ ) was calculated as 32.76 mg/g. The bonding energy ( $E$ ) was calculated to be 0.0007 kJ/mol, which is significantly less than 8 kJ/mol, clearly indicating that the sorption mechanism is predominantly physical in nature. This low bonding energy suggests that van der Waals forces and electrostatic interactions are the primary mechanisms governing the sorption process (Fig 14).



**Fig. 13:** Linearized Temkin adsorption isotherm plot showing the relationship between  $Q_e$  (mg/g) and  $\ln C_e$  for the adsorbent. The regression equation ( $y = 2.3558x + 8.1521$ ) and  $R^2$  value (0.5802) indicate a moderate fit to the Temkin model.



**Fig. 14:** Linearized Dubinin-Radushkevich (D-R) adsorption isotherm plot showing the relationship between  $\ln q_e$  and  $\epsilon^2$ . The regression equation ( $y = -0.4504x + 3.4891$ ) and  $R^2$  value (0.8464) indicate a good fit to the D-R isotherm model, suggesting the nature of adsorption and estimating the mean free energy.

### Overall Isotherm Analysis

The overall isothermal modeling data shown that the Langmuir model provided the best fit ( $R^2 = 99.5\%$ ) for Pb and As sorption using nZVZn, followed by Freundlich ( $R^2 = 89.2\%$ ) and Dubinin-Radushkevich ( $R^2 = 84.6\%$ ) models. The mechanism of sorption was determined to be primarily physical in nature based on the calculated bonding energy values. The physical sorption mechanism can be attributed to the surface properties of nZVZn and the interaction between zero-valent zinc nanoparticles and metal contaminants through electrostatic attraction and surface complexation.

The excellent fit of the Langmuir model suggests monolayer adsorption on homogeneous surface sites, while the favorable Freundlich parameters indicate multilayer adsorption capability. The combination of nZVZn with thiourea modified biochar enhances the overall sorption performance by providing multiple active sites and improving the surface area available for contaminant removal.

Physical sorption mechanisms, while generally less stable than chemisorption, offer advantages in terms of regeneration potential and cost-effectiveness for water treatment applications. The reusability of the nZVZn-biochar composite should be further evaluated through desorption studies to determine the practical applicability of this treatment system.

### Sorption Isotherm Modeling nano-Zerovalent Zinc modified Rice Husk Biochar

Four parameters of nonlinear isotherm models were used to describe the sorption process of lead (Pb) and arsenic (As) using nanoZerovalent Zinc modified Rice Husk Biochar (nZVI-Zn-RHB) namely Langmuir, Freundlich, Temkin and Dubinin-Radushkevich as shown in the figure.

#### Langmuir Model Analysis

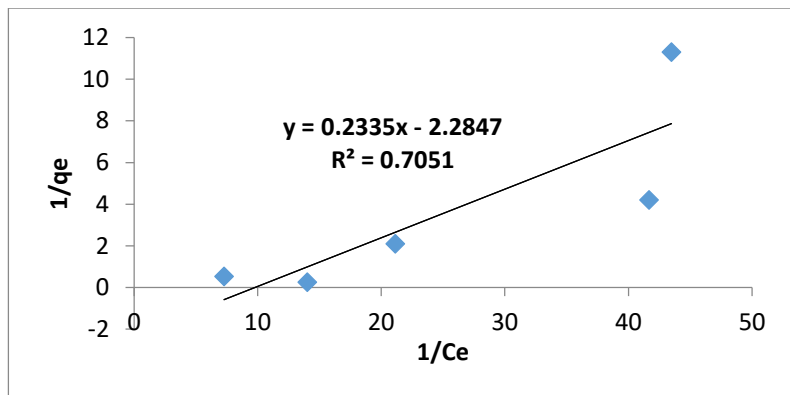
The Langmuir model shown good fit for metal sorption using nZVI-Zn-RHB. The model achieved  $R^2 = 71\%$  with a maximum sorption capacity ( $q_m$ ) value of  $4.28 \text{ mg g}^{-1}$  and Langmuir constant (KL) of  $0.102 \text{ L g}^{-1}$ . The separation factor (RL) values ranged from 0.159 to 0.987, indicating favorable sorption conditions across all initial concentrations tested. Figure showed the best fit Langmuir model for metal sorption onto nZVI-Zn-RHB. The standard error was found to be moderate, demonstrating reasonable model reliability (Fig 15).

The separation factor (RL) was calculated to explore the favorability of metal sorption onto nZVI-Zn-RHB which showed that sorption is favorable by using this zinc-modified biochar sorbent. The RL values consistently between 0 and 1 confirmed that the sorption process is favorable using nZVI-Zn-RHB as sorbent.

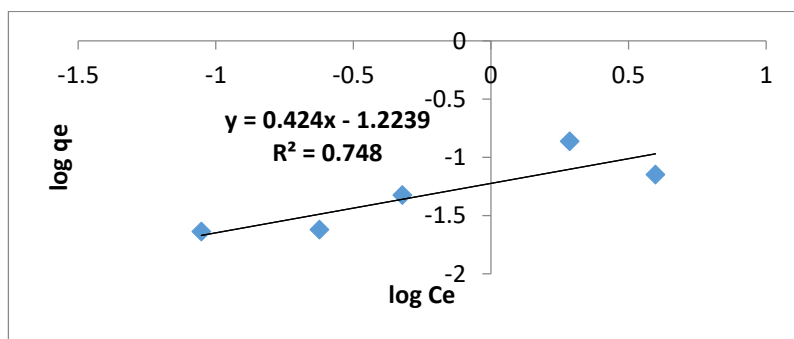
#### Freundlich Model Analysis

The Freundlich model (non-linear) was also employed and shown better correlation compared to the Langmuir model for the experimental data. The model achieved  $R^2 = 75\%$  with a Freundlich constant (Kf) value of  $1.11 \text{ mg}^{1-n} \text{ g}^{-1} \text{ L}^n$  and sorption intensity coefficient (n) of 2.36. The sorption intensity coefficient ( $1/n$ ) was 0.424, which falls between 0 and 1, indicating favorable sorption conditions. The n value greater than 1 ( $n =$

2.36) suggests that the sorption process is favorable and indicates a heterogeneous surface with cooperative adsorption mechanism (Fig 16).



**Fig. 15:** Linearized Langmuir adsorption isotherm plot showing the relationship between  $1/q_e$  and  $1/C_e$  for the adsorbent. The regression equation ( $y = 0.2335x - 2.2847$ ) and  $R^2$  value (0.7051) indicate a moderately good fit to the Langmuir isotherm model, suggesting monolayer adsorption behavior.



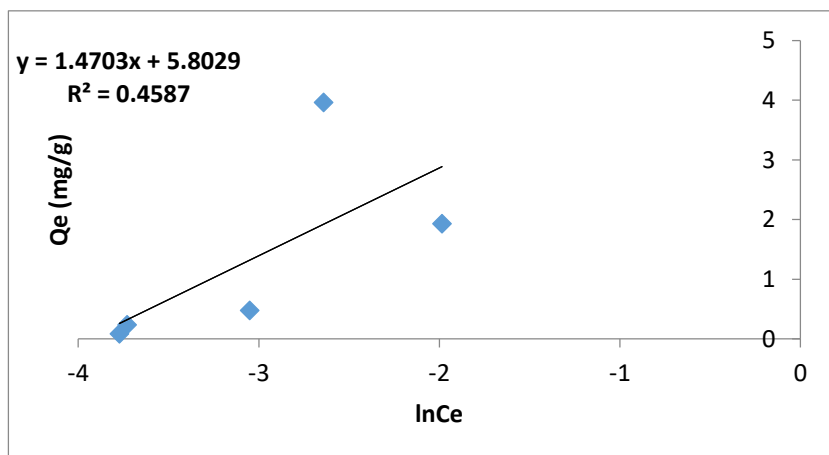
**Fig. 16:** Linearized Freundlich adsorption isotherm plot showing the relationship between  $\log q_e$  and  $\log C_e$  for the adsorbent. The regression equation ( $y = 0.424x - 1.2239$ ) and  $R^2$  value (0.748) indicate a moderately good fit to the Freundlich model, suggesting heterogeneous surface adsorption.

The decrease in the  $1/n$  value explained that the sorption potential remained relatively stable with the increase in the initial concentration of the metals. The standard error of the model was lower compared to the Langmuir model, indicating that the Freundlich model provides better fit for the heterogeneous surface of nZVI-Zn-RHB.

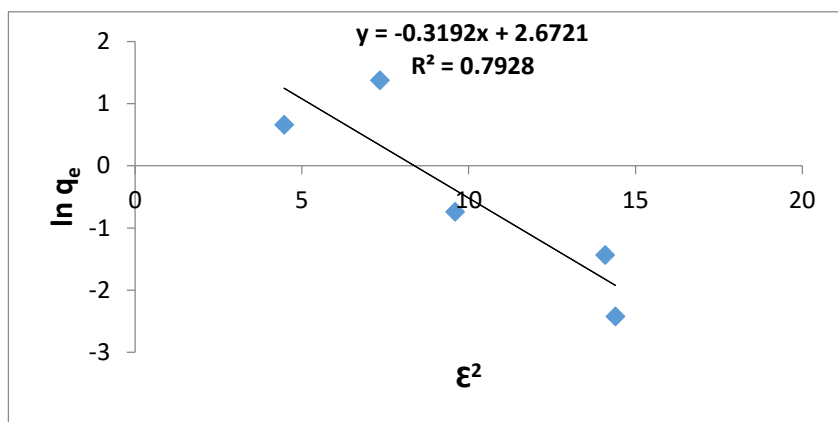
### Temkin Model Analysis

The Temkin model shown moderate correlation with the experimental data, achieving  $R^2 = 46\%$  for the sorption process. The heat of sorption ( $b$ ) was calculated as  $1685.28 \text{ J mol}^{-1}$ , which indicates moderate binding energy between the metal ions and the nZVI-Zn-RHB surface. The Temkin equilibrium binding constant ( $AT$ ) was determined to be  $51.77 \text{ L g}^{-1}$ , suggesting reasonable affinity between the sorbent and sorbate (Fig 17).

Though the  $R^2$  values were lower compared to Langmuir and Freundlich models, the heat of sorption value provides insight into the energetics of the sorption process. The moderate  $b$  value suggests that the sorption involves both physical and weak chemical interactions between the metal ions and the zinc-modified biochar surface, with the zinc nanoparticles potentially providing additional binding sites.



**Fig. 17:** Linearized Temkin adsorption isotherm plot showing the relationship between  $Q_e \text{ (mg/g)}$  and  $\ln C_e$ . The regression equation ( $y = 1.4703x + 5.8029$ ) and  $R^2$  value (0.4587) indicate a weak correlation, suggesting limited applicability of the Temkin model for this adsorption system.



**Fig.18:** Linear plot of  $\ln(q_e)$  versus  $\epsilon^2$  for the Dubinin–Radushkevich (D–R) isotherm model. The slope and intercept of the linear regression equation ( $y = -0.3192x + 2.6721$ ) are used to determine the mean free energy and adsorption capacity, respectively. The coefficient of determination ( $R^2 = 0.7928$ ) indicates the model's fit to the experimental data.

### Dubinin-Radushkevich Model Analysis

The Dubinin-Radushkevich model was employed to determine the nature of the sorption mechanism. The model achieved  $R^2 = 79\%$  with a theoretical saturation capacity ( $q_D$ ) of  $14.47 \text{ mg g}^{-1}$ . Most importantly, the mean free energy of sorption ( $E$ ) was calculated as  $3.10 \text{ kJ mol}^{-1}$ , which is less than  $8 \text{ kJ mol}^{-1}$  (Fig 18).

The bonding energy  $< 8 \text{ kJ mol}^{-1}$  explained the physical nature of sorption mechanism, indicating that the sorption process is primarily governed by physical forces such as van der Waals forces and electrostatic interactions. This bonding energy value was a clear indicator for the physical sorption mechanism, which aligns with previous studies on metal-modified biochar sorbents.

### Overall Isotherm Model Comparison

The overall isothermal modeling data shown that the Dubinin-Radushkevich model provided the best fit for metal sorption with  $R^2 = 79\%$ , followed by Freundlich ( $R^2 = 75\%$ ) and Langmuir ( $R^2 = 71\%$ ) models. The Temkin model showed the lowest correlation ( $R^2 = 46\%$ ) but provided valuable information about the heat of sorption.

The excellent fit of the Dubinin-Radushkevich model suggests that the sorption occurs on a heterogeneous surface with varying energy sites. The good correlation with the Freundlich model also supports the heterogeneous nature of the nZVI-Zn-RHB surface. The favorable separation factors and high correlation coefficients indicate that nZVI-Zn-RHB is an effective sorbent for both lead and arsenic removal from groundwater.

The mechanism of the physical sorption, as confirmed by the Dubinin-Radushkevich model analysis, suggests that the sorption process is reversible, which is advantageous for potential regeneration and reuse of the nZVI-Zn-RHB sorbent. The zinc modification appears to enhance the surface properties of the rice husk biochar, providing additional binding sites through zinc nanoparticles, which contribute to the improved sorption capacity for heavy metals.

These isotherm modeling results demonstrate that nZVI-Zn-RHB is a promising sorbent material for the simultaneous removal of lead and arsenic from contaminated groundwater, with the Dubinin-Radushkevich model best describing the sorption equilibrium behavior.

### Sorption Isotherm Modeling TMBC

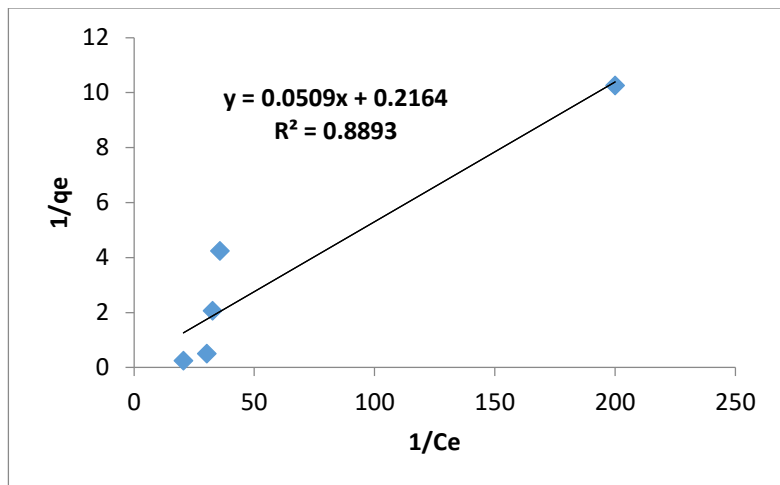
Four parameters of nonlinear isotherm models were used to describe the sorption process of lead (Pb) and arsenic (As) using Thiourea modified Biochar (TMB) namely Langmuir, Freundlich, Temkin and Dubinin-Radushkevich.

### Langmuir Model Analysis

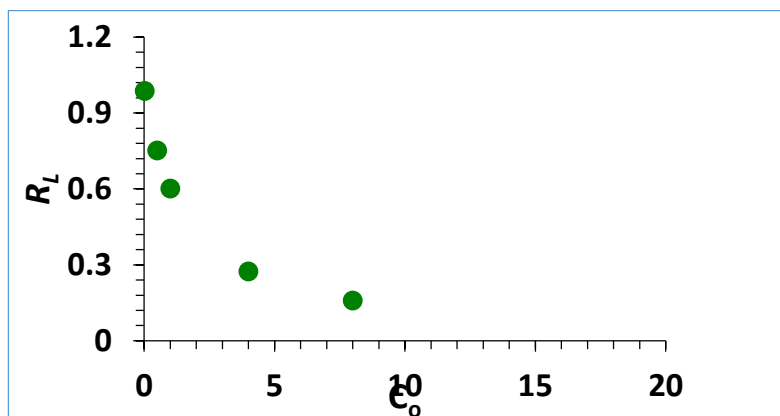
The Langmuir model shown excellent fit for both contaminants using TMB. For lead removal, the model achieved  $R^2 = 89\%$  with a maximum sorption capacity ( $q_m$ ) value of  $19.65 \text{ mg g}^{-1}$  and Langmuir constant ( $KL$ ) of  $0.235 \text{ L g}^{-1}$ . The separation factor ( $RL$ ) values ranged from 0.159 to 0.987, indicating favorable sorption conditions across all initial concentrations tested. Figure 19 showed the best fit Langmuir model for lead sorption onto TMB. The standard error was found to be minimal ( $SE \pm 0.52$ ), demonstrating good model reliability.

For arsenic sorption, similar favorable conditions were observed with RL values consistently between 0 and 1, confirming that the sorption process is favorable using TMB as sorbent. The separation factor (RL) was calculated to explore the favorability of metal sorption onto TMB which showed that sorption is favorable by using this modified biochar sorbent.

The slope (0.0509) and intercept (0.2164) of the linear regression equation ( $y = 0.0509x + 0.2164$ ) are used to determine Langmuir constants related to adsorption capacity and intensity. The correlation coefficient ( $R^2 = 0.8893$ ) indicates a good fit of the model to the experimental data (Fig 20).



**Fig. 19:** Linear plot of  $1/q_e$  versus  $1/C_e$  for the Langmuir isotherm model.



**Fig. 20:** Variation of the separation factor (RL) with initial adsorbate concentration ( $C_0$ ) for the Langmuir isotherm model. The plot shows a decreasing trend of RL values with increasing  $C_0$ , indicating favorable adsorption ( $0 < RL < 1$ ) across the studied concentration range.

### Freundlich Model Analysis

The Freundlich model (non-linear) was also employed and shown good correlation for the experimental data. For lead sorption, the model achieved  $R^2 = 66\%$  with a Freundlich constant ( $K_f$ ) value of  $34.04 \text{ mg}^{1-n} \text{ g}^{-1} \text{ L}^n$  and sorption intensity coefficient ( $n$ ) of 2.11. The sorption intensity coefficient ( $1/n$ ) was 0.475, which falls between 0 and 1, indicating favorable sorption conditions. The  $n$  value greater than 1 ( $n = 2.11$ ) suggests that the sorption process is favorable and indicates a cooperative adsorption mechanism.

The decrease in the  $1/n$  value explained that the sorption potential remained relatively stable with the increase in the initial concentration of the metals. The standard error of the model was moderate compared to the Langmuir model, indicating that while the Freundlich model provides reasonable fit, the Langmuir model better describes the sorption behavior (Fig 21).

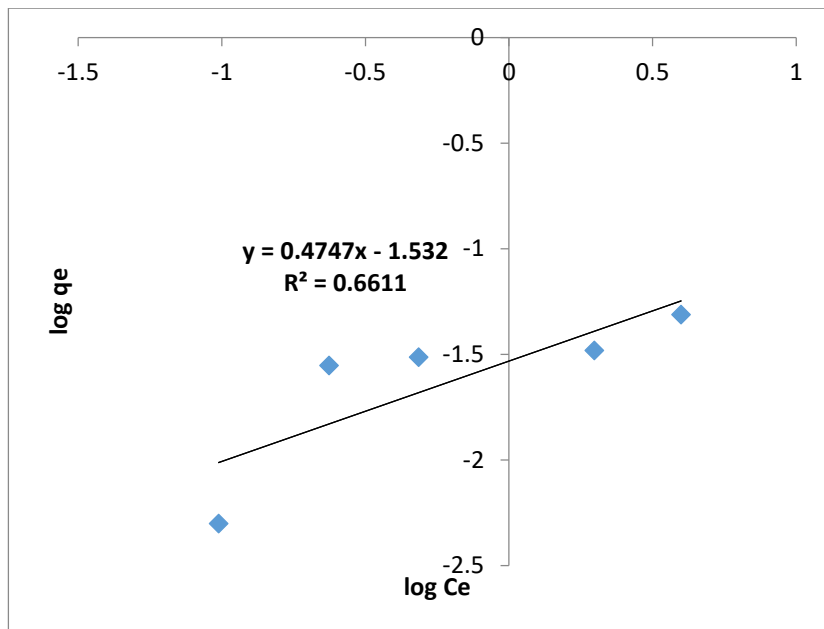
The slope (0.4747) represents the adsorption intensity ( $1/n$ ), and the intercept ( $-1.5382$ ) corresponds to  $\log K_F$ , where  $K_F$  is the Freundlich constant. The correlation coefficient ( $R^2 = 0.6611$ ) indicates a moderate fit of the model to the experimental data.

### Temkin Model Analysis

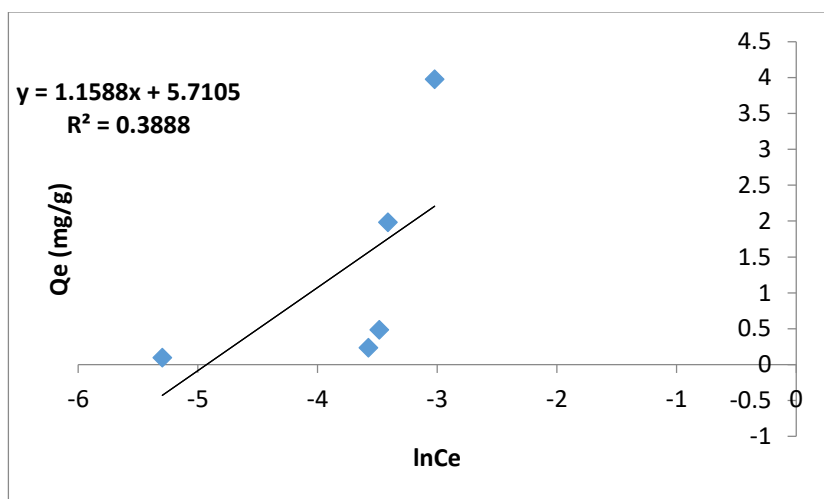
The Temkin model shown moderate correlation with the experimental data, achieving  $R^2 = 39\%$  for the sorption process. The heat of sorption ( $b$ ) was calculated as  $2138.31 \text{ J mol}^{-1}$ , which indicates moderate binding energy between

the metal ions and the TMB surface. The Temkin equilibrium binding constant ( $AT$ ) was determined to be  $302.02 \text{ L g}^{-1}$ , suggesting reasonable affinity between the sorbent and sorbate (Fig 22).

Though the  $R^2$  values were lower compared to Langmuir and Freundlich models, the heat of sorption value provides insight into the energetics of the sorption process. The moderate  $b$  value suggests that the sorption involves both physical and weak chemical interactions between the metal ions and the thiourea-modified biochar surface.



**Fig. 21:** Linear plot of  $\log q_e$  versus  $\log C_e$  for the Freundlich isotherm model.



**Fig. 22:** Linear plot of  $q_e$  versus  $\ln C_e$  for the Temkin isotherm model.

The slope (1.1588) and intercept (5.7105) of the linear regression equation ( $y = 1.1588x + 5.7105$ ) are used to calculate Temkin constants related to adsorption heat and equilibrium binding. The low correlation coefficient ( $R^2 = 0.3888$ ) indicates a poor fit of the model to the experimental data.

#### Dubinin-Radushkevich Model Analysis

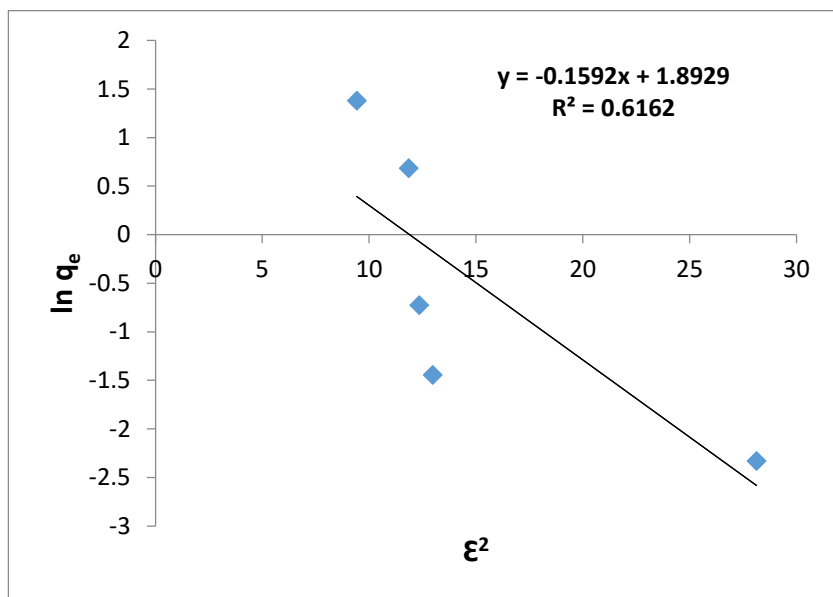
The Dubinin-Radushkevich model was employed to determine the nature of the sorption mechanism. The model achieved  $R^2 = 62\%$  with a theoretical saturation capacity ( $q_D$ ) of  $6.64 \text{ mg g}^{-1}$ . Most importantly, the mean free energy of sorption ( $E$ ) was calculated as  $4.39 \text{ kJ mol}^{-1}$ , which is less than  $8 \text{ kJ mol}^{-1}$  (Fig 23).

The bonding energy  $< 8 \text{ kJ mol}^{-1}$  explained the physical nature of sorption mechanism, indicating that the sorption process is primarily governed by physical forces such as van der Waals forces and electrostatic

interactions. This bonding energy value was a clear indicator for the physical sorption mechanism, which aligns with previous studies on biochar-based sorbents.

### Overall Isotherm Model Comparison

The overall isothermal modeling data shown that the Langmuir model provided the best fit for metal sorption with  $R^2 = 89\%$ , followed by Freundlich ( $R^2 = 66\%$ ) and Dubinin-Radushkevich ( $R^2 = 62\%$ ) models. The Temkin model showed the lowest correlation ( $R^2 = 39\%$ ) but provided valuable information about the heat of sorption.



**Fig. 23:** Linear plot of  $\ln q_e$  versus  $\epsilon^2$  for the Dubinin-Radushkevich (D-R) isotherm model. The slope ( $-0.1592$ ) and intercept ( $1.8929$ ) of the regression line are used to calculate the mean free energy and adsorption capacity. The correlation coefficient ( $R^2 = 0.6162$ ) suggests a moderate fit of the model to the experimental data.

The excellent fit of the Langmuir model suggests that the sorption occurs primarily on homogeneous surface sites with monolayer coverage. The favorable RL values and high correlation coefficient indicate that TMBC is an effective sorbent for both lead and arsenic removal from groundwater.

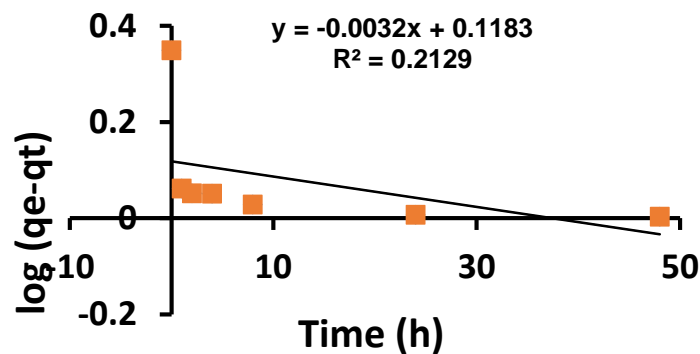
The mechanism of the physical sorption, as confirmed by the Dubinin-Radushkevich model analysis, suggests that the sorption process is reversible, which is advantageous for potential regeneration and reuse of the TMBC sorbent. The thiourea modification appears to enhance the surface properties of the biochar, providing additional binding sites through sulfur and nitrogen functional groups, which contribute to the improved sorption capacity for heavy metals.

These isotherm modeling results demonstrate that TMBC is a promising sorbent material for the simultaneous removal of lead and arsenic from contaminated groundwater, with the Langmuir model best describing the sorption equilibrium behavior.

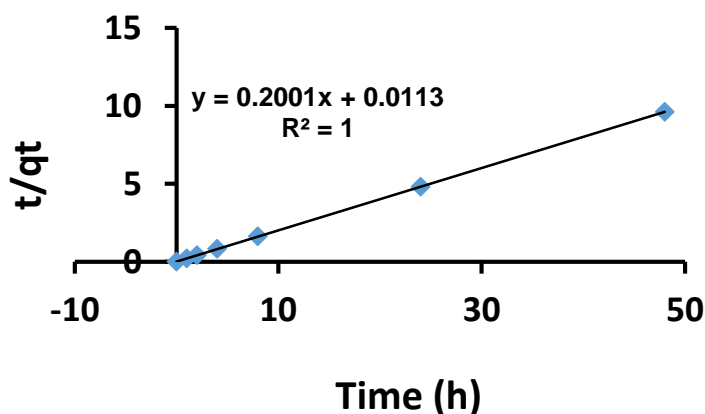
### Kinetic Modelling Results Interpretation Lead & Arsenic Removal Kinetics

Kinetic modelling was used to evaluate the rate of lead sorption on different adsorbent materials including thiourea-modified biochar, nano zero-valent zinc (nZn), rice husk biochar (RH-BC), and rice husk biochar with nano zero-valent zinc (RH-BCnZn) under different time intervals. For these, two kinetic models - pseudo-first order and pseudo-second order - were employed to explore the rate of reaction.

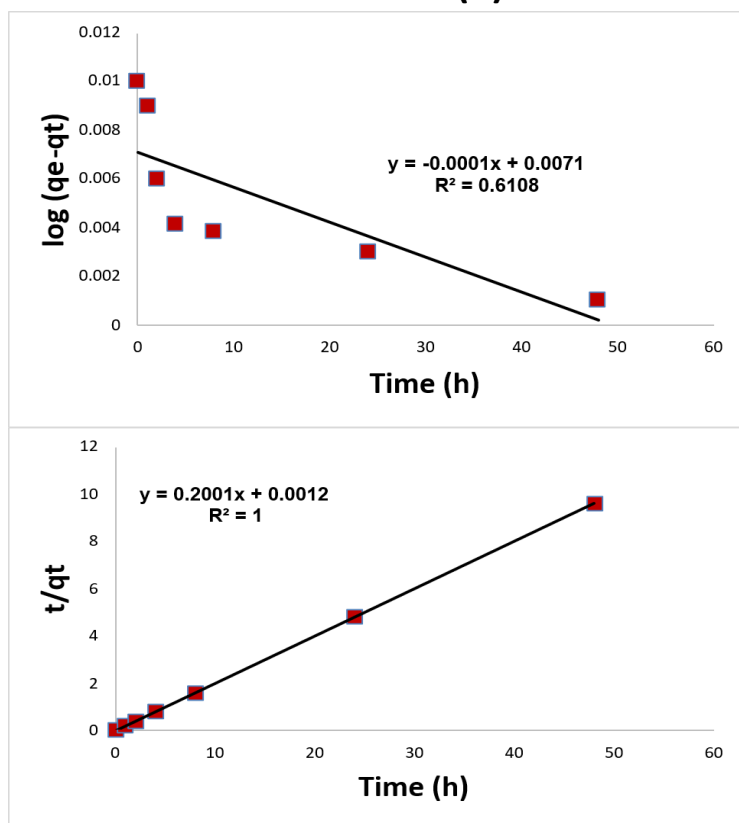
All adsorbent materials showed best fit using pseudo-second order model with  $R^2 \geq 99.99\%$  while maximum value of  $q_e$  was observed with thiourea-modified biochar followed by nZn, achieving 5.025 and 4.998 mg/g respectively. Both RH-BC and RH-BCnZn demonstrated comparable adsorption capacities of 4.998 and 4.960 mg/g respectively. In pseudo-first order model, RH-BCnZn showed the highest correlation with  $R^2 = 63.99\%$  while other adsorbents were below  $R^2 = 61\%$  (thiourea-modified biochar:  $R^2 = 49.03\%$ , nZn:  $R^2 = 61.08\%$ , RH-BC:  $R^2 = 21.29\%$ ). The values of  $q_e$  were close to the experimental values which also supports the maximum fit for pseudo-second order model. However,  $q_e$  values in the pseudo-first order model showed significant deviations from experimental data, particularly for thiourea-modified biochar where the calculated value was approximately 2.5 times lower than the pseudo-second order prediction (Fig 24-31).



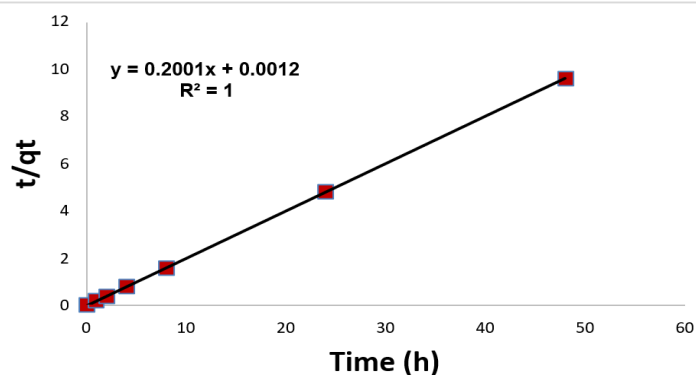
**Fig. 24:** Pseudo-first-order kinetics model plot showing the relationship between  $\log (q_e - q_t)$  and time (h). The regression equation ( $y = -0.0032x + 0.1183$ ) and low  $R^2$  value (0.2129) indicate a poor fit, suggesting that the adsorption process does not follow the pseudo-first-order kinetic model effectively.



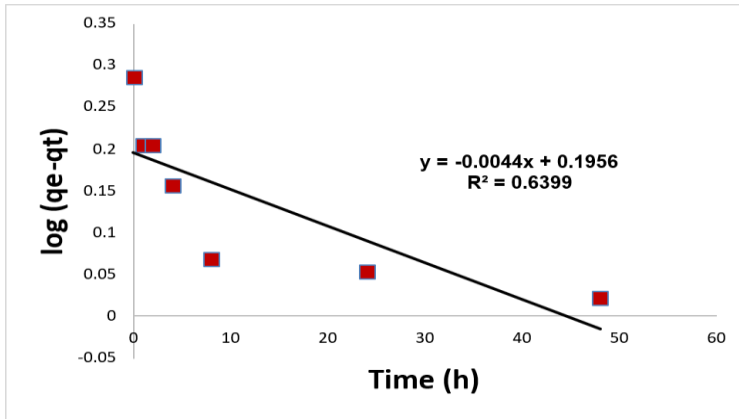
**Fig. 25:** Pseudo-second-order kinetic model plot showing the relationship between  $t/q_t$  and time (h). The linear regression equation ( $y = 0.2001x + 0.0113$ ) with a perfect  $R^2$  value of 1 indicates an excellent fit, suggesting that the adsorption process follows the pseudo-second-order kinetic model accurately.



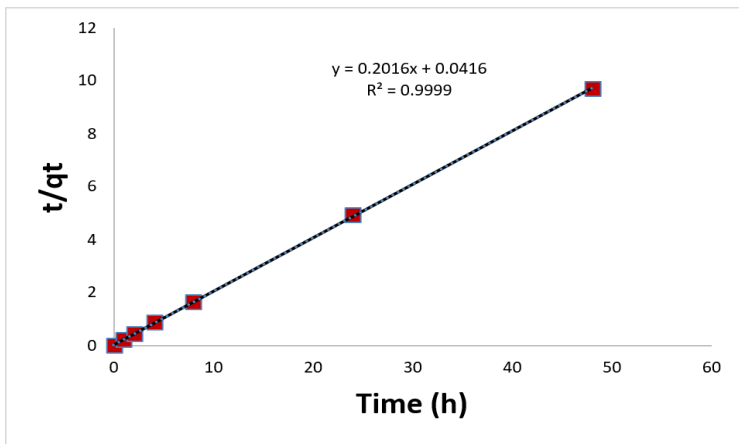
**Fig. 26:** Pseudo-first-order kinetic model plot of  $\log (q_e - q_t)$  versus time (h). The linear regression equation ( $y = -0.0001x + 0.0071$ ) and coefficient of determination ( $R^2 = 0.6108$ ) indicate a moderate fit, suggesting that the adsorption process does not strongly follow pseudo-first-order kinetics.



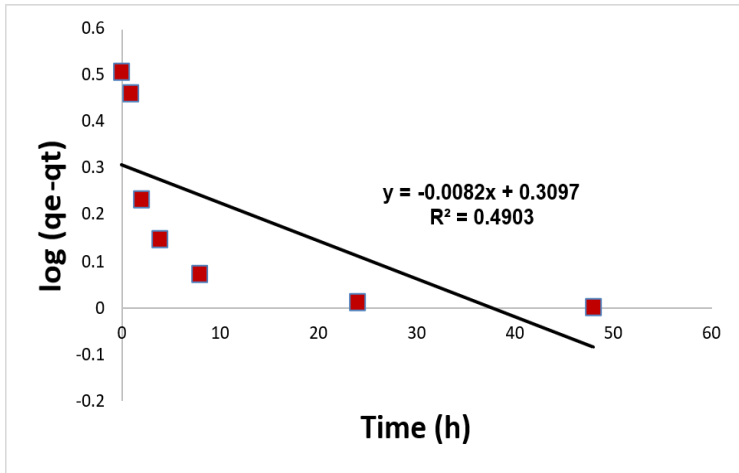
**Fig. 27:** Pseudo-second-order kinetic model plot of  $t/q_t$  versus time (h). The linear regression equation ( $y = 0.2001x + 0.0012$ ) and coefficient of determination ( $R^2 = 1$ ) indicate an excellent fit, suggesting that the adsorption process follows pseudo-second-order kinetics perfectly.



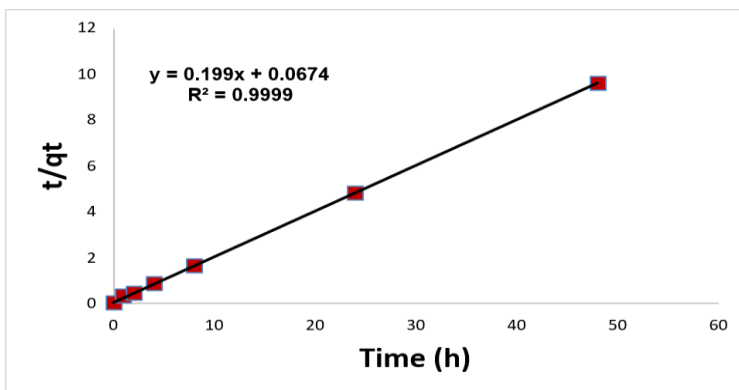
**Fig. 28:** Pseudo-first-order kinetic model plot of  $\log(q_e - q_t)$  versus time (h). The linear regression equation ( $y = -0.0044x + 0.1956$ ) and coefficient of determination ( $R^2 = 0.6399$ ) indicate a moderate fit, suggesting that the adsorption process partially follows pseudo-first-order kinetics.



**Fig. 29:** Pseudo-second-order kinetic model plot of  $t/q_t$  versus time (h). The linear regression equation ( $y = 0.2016x + 0.0416$ ) and coefficient of determination ( $R^2 = 0.9999$ ) indicate an excellent fit, suggesting that the adsorption process follows pseudo-second-order kinetics closely.



**Fig. 30:** Intraparticle diffusion kinetic model plot of  $\log(q_e - q_t)$  versus time (h). The linear regression equation ( $y = -0.0082x + 0.3097$ ) and coefficient of determination ( $R^2 = 0.4903$ ) indicate a moderate fit, suggesting that intraparticle diffusion is not the sole rate-controlling step in the adsorption process.



**Fig. 31:** Pseudo-second-order kinetic model plot of  $t/q_t$  versus time (h). The linear regression equation ( $y = 0.199x + 0.0674$ ) and coefficient of determination ( $R^2 = 0.9999$ ) indicate a strong fit, suggesting that the adsorption process follows pseudo-second-order kinetics accurately.

## 4 | DISCUSSION

The SEM analysis showed that biochar has a high heterogeneous surface structure. Moreover, it possesses many pores and cavities. These features promote metal ion adsorption. The rough and uneven surface and high surface area are vital for heavy metal adsorption. This was shown by the use of agricultural waste-derived biochar. (Phiri *et al.*, 2024). The nZn particles that were made have round shapes with sizes of 20 to 80 nm. The reactivity of these dimensions for heavy metals remediation is high owing to their surface to volume ratio (Liu *et al.*, 2022).

The nZn-BC composite showed even distribution of nanoparticles into the biochar matrix, preventing agglomeration of nanoparticles and maximizing the active surface area. It can help to adsorb and redox that affirms the study by Ghandali *et al.* (2024) Thiourea modification led to the introduction of sulfur and nitrogen functional groups on the biochar's surface that enhanced its chemical reactivity for selective binding of heavy metals (Shaheen *et al.*, 2022).

Through the sorption isotherm and kinetic model analyses, we inferred the adsorption mechanism. According to the Langmuir model, most materials underwent adsorption due to monolayer adsorption on a homogenous site. nZn and TMBC had R<sup>2</sup> values were 99.5% and 89% respectively. This suggests that adsorbent has the same active binding sites with no lateral interactions between the adsorbed species (Ahmad *et al.*, 2018). The high correlation value (R<sup>2</sup> = 88.05%) of the Langmuir model suggests that RH-BC was adopted as a favorable monolayer adsorption agent similar to that in earlier studies (Inyang *et al.*, 2016).

The Dubinin-Radushkevich model gave the best fit for the nZn-modified biochar (nZn-RHB) indicating a heterogeneous surface with energy types. Based on the mean free energy (E = 3.10 kJ/mol) it can be inferred that the adsorption of the adsorbent was governed by physical sorption mechanism which was also substantiated with van der Waals forces and electrostatic interactions were also at play. The correlation was moderate for Freundlich (R<sup>2</sup> = 75% – 89.2%) and the corresponded multilayer adsorption at higher concentrations according to Foo & Hameed (2010).

The results of kinetic modeling suggested that the pseudo-second-order model best describes the adsorption process for all the adsorbents as the R<sup>2</sup> values for lead removal were greater than or equal to 99.99 per cent which indicates that the adsorption process occurs through chemisorption by electron transfer and this is the rate slow step (Ho & McKay, 1999). Thiourea-modified biochar (TMB) has the highest adsorption ability of all the adsorbents prepared (q<sub>e</sub> = 5.025 mg/g). The presence of sulphur and nitrogen functional groups on urea gave TMB a strong binding affinity towards the dye molecule. nZn proved to be effective, confirming the efficacy of nano zerovalent zinc for providing active sites for metal complexation.

The adsorption capacity of biochar and biochar composites (RH-BC, nZn-RHB) was in the order of 4.28 mg/g-5.025 mg/g with the maximum capacity (19.65 mg/g) of TMB, showing the synthesis effects of biochar and thiourea modification (Wang *et al.* 2019). According to the pseudo-first-order model the data poorly fitted as depicted from the R<sup>2</sup> values (R<sup>2</sup> < 64%). This confirms that the mechanism of adsorption is complex and it is not encountering resistance from mass transfer but via chemical interactions.

According to the Temkin model the binding energies were moderate (1052–2138 J/mol) indicating physical and weak chemical interactions. The results indicate that while physical sorption is the more important process, the groups on the modified biochar enhance lead and arsenic sorption capacity.

The TMB and other composite materials were seen to be highly efficacious in the removal of lead and arsenic. Two major properties of many adsorbents are reversibility of the sorption process and the heterogeneous nature of their surfaces. These adsorbents may take up several metal species and may be suitable for the treatment of complex polluted water systems. This study enhances the knowledge of adsorbent materials, and it offers a useful, ecological solution for water treatment.

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**Conflicts of Interest:** The authors confirm no conflicts of interest

**Authors' Contribution:** Sidra Chaudary designed the study, conducted the literature review, performed the characterization of materials and analytical data evaluation, prepared the associated figures and graphs, drafted and critically revised the manuscript, and approved the final version.

**Generative AI Statements:** The authors declare that this manuscript has been written without the use of generative artificial intelligence tools.

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